

Thermodynamics 1 (MEP 261)

Quiz 3 ( 20 Marks)

Model Answer

Class ZA, Date: March 17, 2012

Name:

University ID:

Complete the following table for refrigerant-134a ( 16 Marks).

Specify each state on  $T$ - $s$  diagram ( 4 Marks).

<i>Point</i>	<i>T, °C</i>	<i>p, kPa</i>	<i>u, kJ/kg</i>	<i>v, m<sup>3</sup>/kg</i>	<i>x</i>	Phase description
1	<b>-10</b>	<b>300</b>				
2	<b>20</b>			<b>0.012</b>		
3		<b>120</b>				<b>Saturated vapor</b>
4	<b>75</b>	<b>700</b>				

**Solution:**

**For refrigerant-134a:**

State 1:  $T = -10$  °C,  $p = 300$  kPa , From Table A-12 (Saturated **refrigerant-134a** -Pressure table),

For  $p = 280$  kPa,  $T_{sat} = -1.25$  °C,

For  $p = 320$  kPa,  $T_{sat} = 2.46$  °C,

Hence, for  $p = 300$  kPa,  $T_{sat} = -1.25 + 2.46$  °C =  $1.21$  °C =  $0.605$  °C

As  $T$  ( $= -10$  °C)  $<$   $T_{sat}$  ( $= 0.605$  °C), Hence, State 1 is compressed (subcooled) liquid,

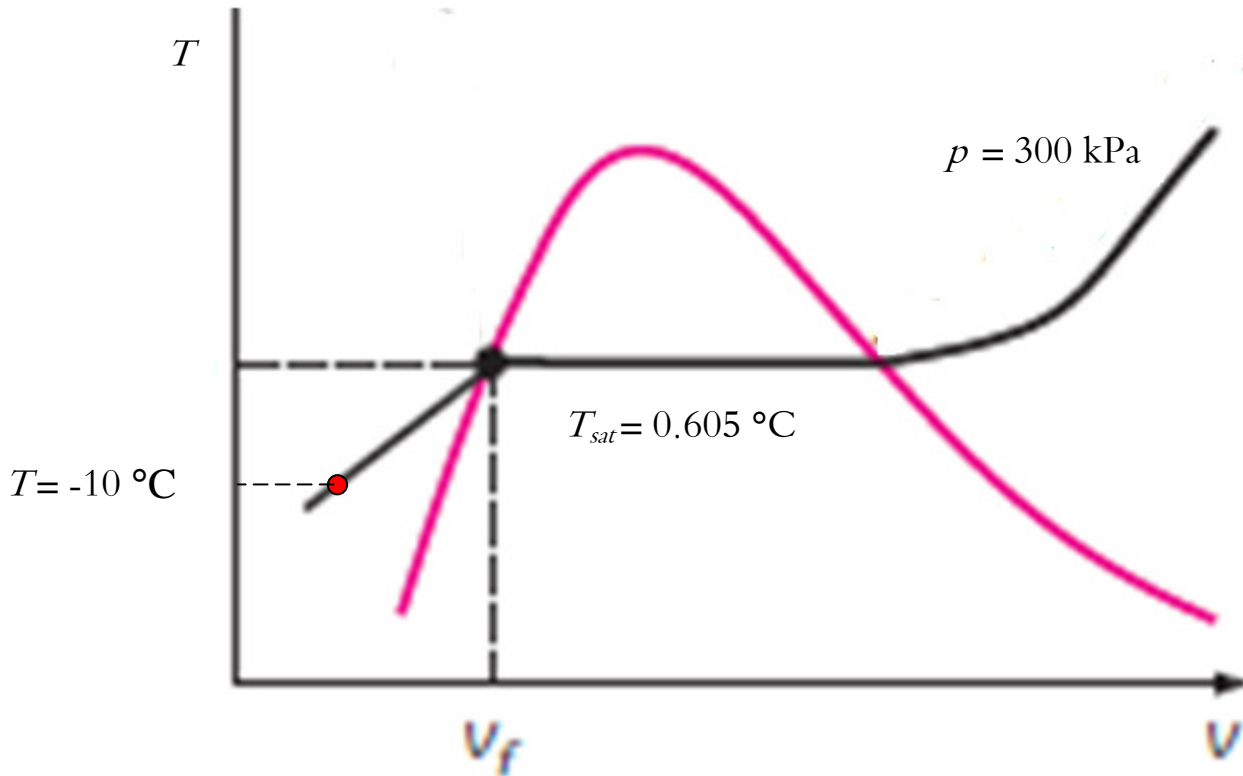
Hence, conditions are nearly the same as those at Saturated liquid corresponding to  $T = -10.0$  °C.

Hence, From Table A-11, corresponding to  $T = -10$  °C

$T, \text{ }^\circ\text{C}$	$v_f, \text{ m}^3/\text{kg}$	$u_f, \text{ kJ/kg}$	$h_f, \text{ kJ/kg}$	$s_f, \text{ kJ/kg.K}$
-10	0.0007535	38.40	38.55	0.15504

$$v = v_f = 0.0007535 \text{ m}^3/\text{kg} \ \& \ u = u_f = 38.40 \text{ kJ/kg}$$

$$h = h_f = 38.5 \text{ kJ/kg} \ \& \ s = s_f = 0.15504 \text{ kJ/kg.K}$$



State 2:  $T = 20\text{ }^{\circ}\text{C}$ ,  $v = 0.012\text{ m}^3/\text{kg}$ , From Table A-11 (Saturated refrigerant-134a -Temperature table)

For  $T = 20\text{ }^{\circ}\text{C}$ ,  $p_{sat} = 572.07\text{ kPa}$ ,  $v_f = 0.0008161\text{ m}^3/\text{kg}$ ,  $v_g = 0.035969\text{ m}^3/\text{kg}$ ,  $u_f = 78.86\text{ kJ/kg}$ ,  $u_{fg} = 162.16\text{ kJ/kg}$ ,  $u_g = 241.02\text{ kJ/kg}$ .

As  $v_f (= 0.0008161\text{ m}^3/\text{kg}) < v (= 0.012\text{ m}^3/\text{kg}) < v_g (= 0.035969\text{ m}^3/\text{kg})$

Hence, state 2 is saturated liquid-vapor mixture

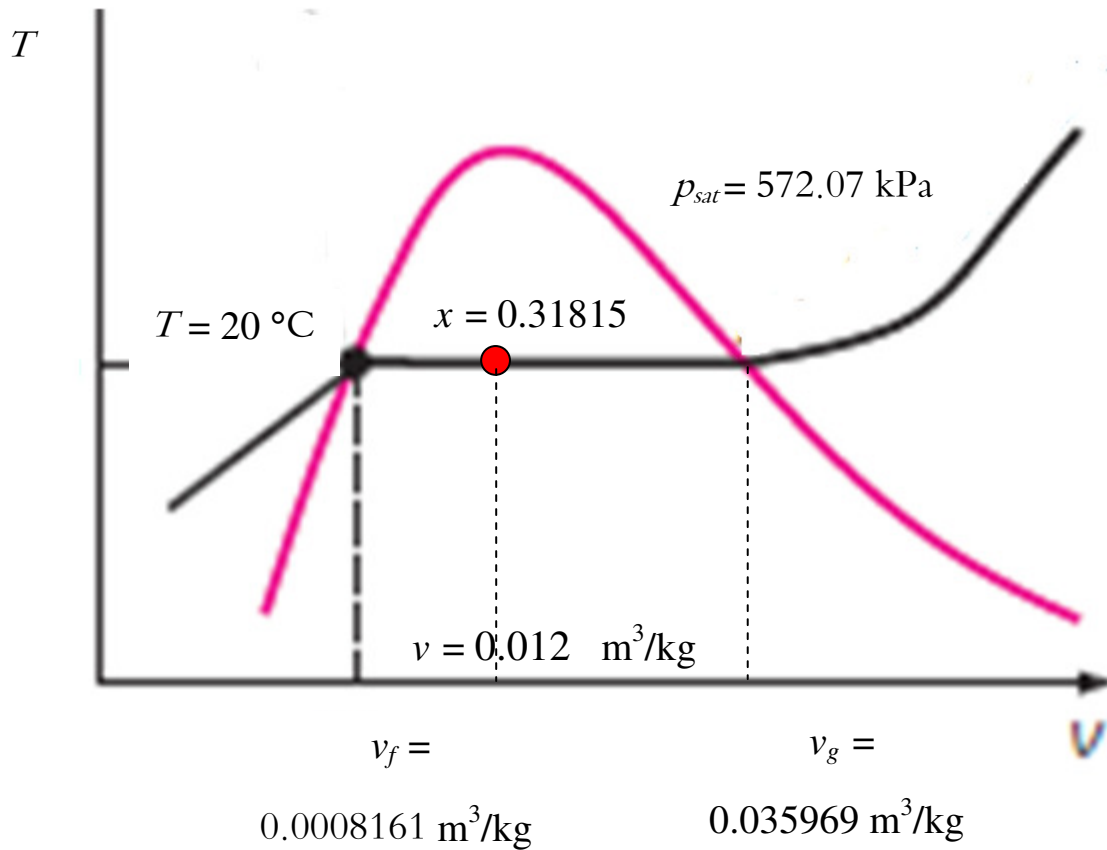
$$x = \frac{v - v_f}{v_g - v_f}$$

Hence,

$$x = \frac{0.012 - 0.0008161}{0.035969 - 0.0008161}$$

Hence,  $x = 0.31815$ ,

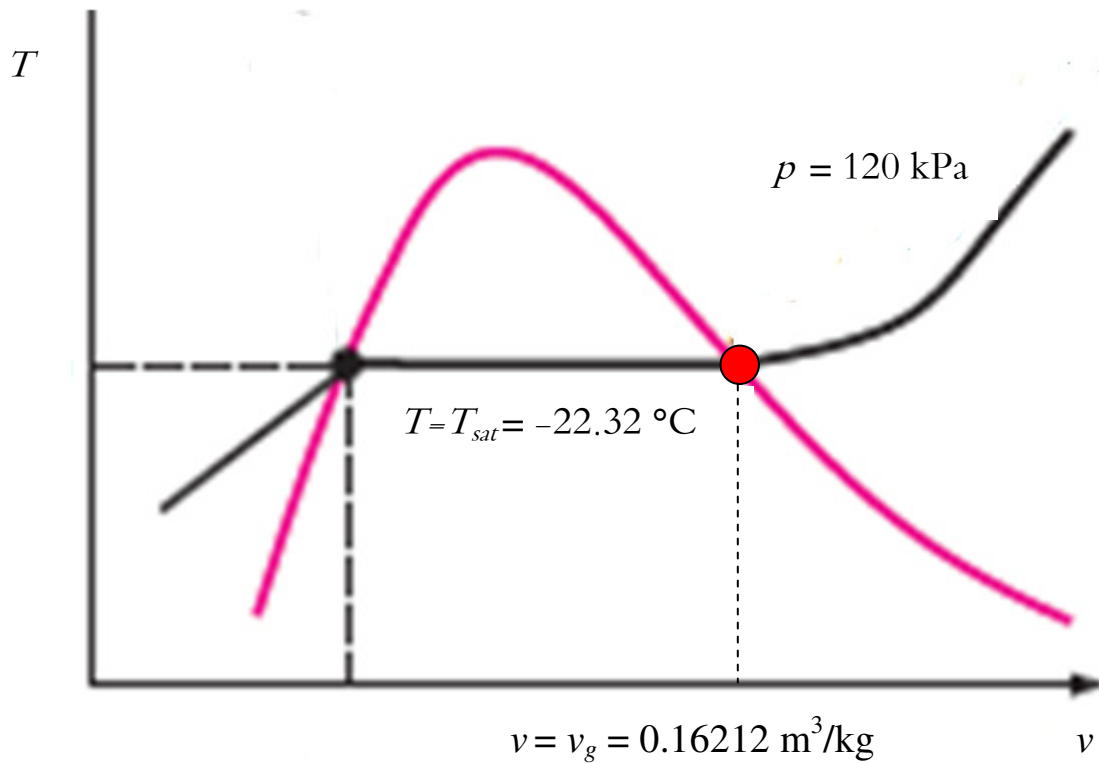
$$u = u_f + x u_{fg} = 78.86 \text{ kJ/kg} + 0.31815 \times 162.16 \text{ kJ/kg} = 130.4512 \text{ kJ/kg}$$



State 3:  $p = 120 \text{ kPa}$ , Saturated vapor,  $x = 1$ ;

**From Table A-12** (Saturated **refrigerant-134a** -Pressure table),

For  $p = 120 \text{ kPa}$ ,  $T = T_{sat} = -22.32 \text{ }^\circ\text{C}$ ,  $v = v_g = 0.16212 \text{ m}^3/\text{kg}$ ,  $u = u_g = 217.51 \text{ kJ/kg}$ .



State 4:  $T = 75 \text{ }^\circ\text{C}$ ,  $p = 700 \text{ kPa}$ ,

**From Table A-12** (Saturated **refrigerant-134a** -Pressure table),

$$T_{sat \text{ at } p = 700 \text{ kPa}} (=26.69 \text{ }^\circ\text{C}),$$

As  $T (=75 \text{ }^\circ\text{C}) > T_{sat \text{ at } p = 700 \text{ kPa}} (=26.69 \text{ }^\circ\text{C})$ , hence state 4 is superheated vapor.

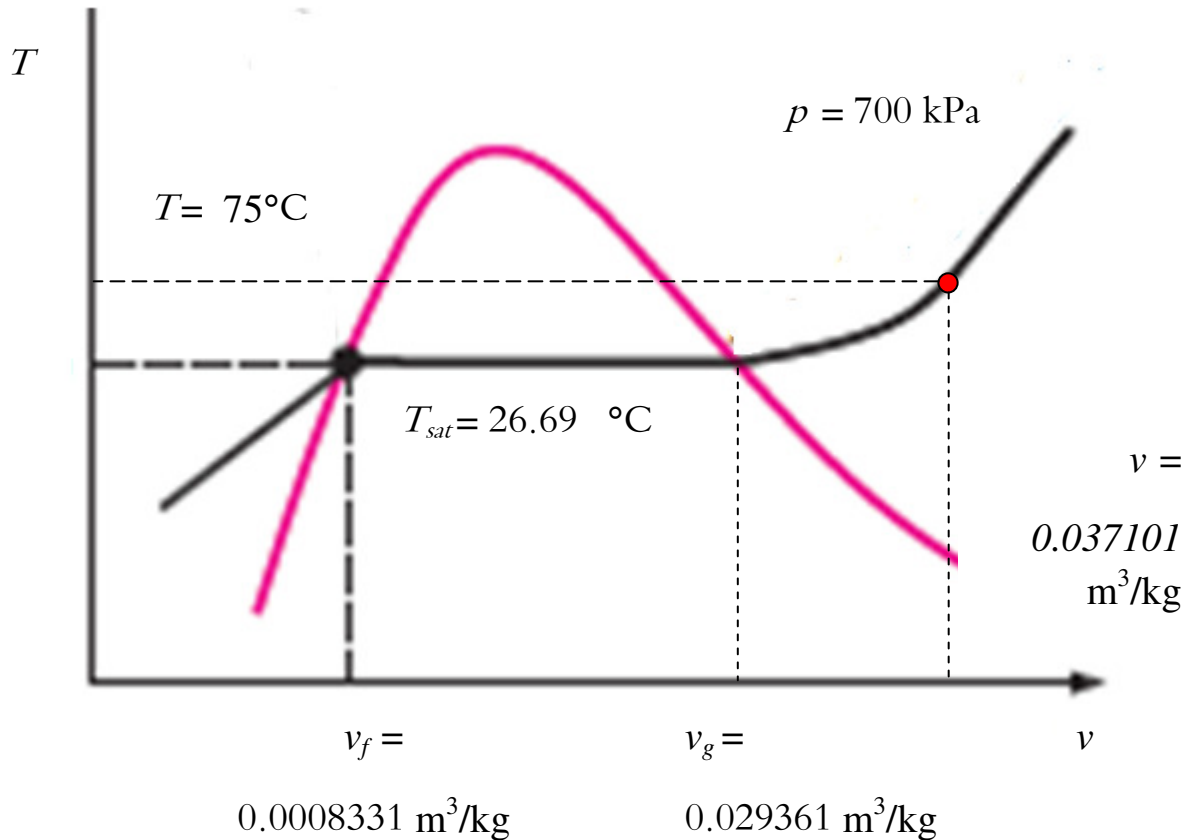
Hence, From Table A-13, Superheated **refrigerant-134a**

For  $p = 700 \text{ kPa}$  ( $=0.7 \text{ MPa}$ ),  $T = 70 \text{ }^\circ\text{C}$ ,  $v = 0.036373 \text{ m}^3/\text{kg}$  &  $u = 282.87 \text{ kJ/kg}$

For  $p = 700 \text{ kPa}$  ( $=0.7 \text{ MPa}$ ),  $T = 80 \text{ }^\circ\text{C}$ ,  $v = 0.037829 \text{ m}^3/\text{kg}$  &  $u = 291.80 \text{ kJ/kg}$

Hence,

For  $p = 700 \text{ kPa}$  ( $=0.7 \text{ MPa}$ ),  $T = 75 \text{ }^\circ\text{C}$ ,  $v = (0.036373 + 0.037829)/2 = 0.037101 \text{ m}^3/\text{kg}$  &  $u = (282.87 + 291.80)/2 = 287.3 \text{ kJ/kg}$



*Solution:*

<i>Point</i>	<i>T, °C</i>	<i>p, kPa</i>	<i>u, kJ/kg</i>	<i>v, m<sup>3</sup>/kg</i>	<i>x</i>	<i>Phase description</i>
1	<b>-10</b>	<b>300</b>	38.40	0.0007535	-	<i>Compressed (subcooled) liquid</i>
2	<b>20</b>	572.07	130.4512	<b>0.012</b>	0.31815	<i>Saturated liquid- vapor mixture</i>
3	-22.32	<b>120</b>	217.51	0.16212	1.0	<b>Saturated vapor</b>
4	<b>75</b>	<b>700</b>	287.3	0.037101	-	<i>Superheated vapor</i>